

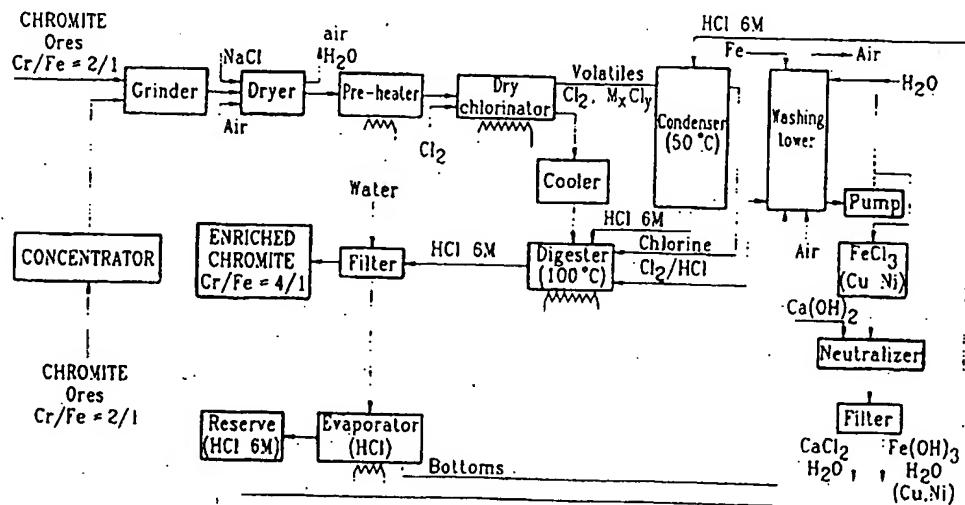


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(71) Applicant (for all designated States except US):	UG PLUS INTERNATIONAL INC. [CA/CA]; 550 Chambly, Sherbrooke, Quebec J1J 2Y2 (CA).	
(72) Inventors; and		
(75) Inventors/Applicants (for US only):	LALANCETTE, Jean-Marc [CA/CA]; 470 Irène-Couture, Sherbrooke, Quebec J1L 1J4 (CA). BERGERON, Mario [CA/CA]; 1253 de Fenouillet, Cap-Rouge, Quebec G1Y 2Y6 (CA). BOSSE, François [CA/CA]; 155 Frédéric Hébert, Rouyn-Noranda, Quebec J9X 1V8 (CA). CLERK, Cyril [CA/CA]; 390 Chemin des Patriotes, North, Mont-St.-Hilaire, Quebec J3H 3H6 (CA).	
(74) Agents:	DUBUC, Jean et al.; Goudreau Gage Dubuc & Martineau Walker, The Stock Exchange Tower, Suite 3400, 800 Square Victoria, P.O. Box 242, Montreal, Quebec H4Z 1E9 (CA).	

(54) Title: PROCESS FOR OBTAINING CHROMIUM ENRICHED CHROMITE FROM CHROMITE ORES



(57) Abstract

A process for obtaining chromium enriched chromite from chromite ores comprising the steps of: dry chlorinating the ores at a temperature between 400 °C and 750 °C to produce a chlorinated substrate containing acid soluble ferric oxide, acid soluble ferric chloride and acid insoluble chromium enriched chromite; digesting the chlorinated substrate with hydrochloric acid to dissolve the ferric oxide and the ferric chloride; and recovering the chromium enriched chromite.

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TITLE OF THE INVENTION

Process for obtaining chromium enriched chromite from chromite ores.

FIELD OF THE INVENTION

5 The present invention relates to a process for obtaining chromium enriched chromite from chromite ores or chromite concentrates.

BACKGROUND OF THE INVENTION

The production of metallic chromium is an
10 important metallurgical process, this metal being an essential component in high performance alloys and in apparatuses exposed to corrosion. The elaboration of elemental chromium is made from the chromium III oxide, Cr₂O₃. If a crude form of chromium is desired, such as
15 in the ferrochrome master alloys, the chromite, FeO • Cr₂O₃, which is the most common occurrence of chromium in nature, is directly reduced with carbon in an arc furnace to give an iron-chromium alloy described by the following equation:
20 FeO • Cr₂O₃ + 4C → 4CO + Fe + 2Cr

On the other hand, in applications where chromium must be of high purity, such as in electrochemical technologies, pure Cr₂O₃ is required as a starting material and the production of the free metal
5 is done by reaction with aluminum as described by the following equation.



This aluminothermic reaction is quite exothermic (130 Kcal/mole) and gives fused alumina as a
10 secondary product. Therefore, the elaboration of chromium III oxide, either as chromite of high chromium content or as purified Cr₂O₃, is an important step in the production of elemental chromium of good quality.

At present, the production of chromium III oxide consists of a rather elaborate process wherein chromite is used as the starting material. The main steps of this process consist in first fusing the chromite in the hearth of a reverberatory furnace with the addition of alkali hydroxide or carbonate and burned
15 lime. In this way, the chromium is transformed into chromate, through the oxidizing action of the furnace flame, in the presence of an excess of oxygen. The chromate leached out with water is converted to
20

dichromate by the addition of acid. After separation of more sparingly soluble compounds, the dichromate is deposited from the concentrated solution in a sufficiently pure state. Pure chromium III oxide is then 5 obtained by reduction with carbon (see H. REMY, Treatise on Inorganic Chemistry, Vol. II, p. 155, Elsevier Publishing Company, 1956).

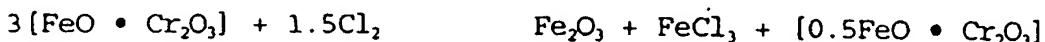
It will be readily seen that such a complex procedure makes the resulting chromium III oxide an 10 expensive commodity.

SUMMARY OF THE INVENTION

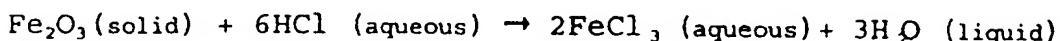
In the course of a study of the recovery of trace amounts of platinum and related metals from chromite (see applicant's copending international application PCT/CA96/00060 filed January 30, 1996), the inventors have been led to use chlorine as a reagent for the extraction of these precious metals from the chromite. The presence of a trace amount of sodium chloride in the chromite seems to facilitate the 15 reactions. Although chlorine turned out to be a very 20 selective reagent for the recovery of platinoids, leaving

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most of the chromite unaltered, the inventors have noted that, by appropriate operating conditions, a significant amount of the iron oxide present in the chromite ($\text{FeO} \cdot \text{Cr}_2\text{O}_3$) in the presence of NaCl could be oxidized to 5 hematite, thus increasing the Cr/Fe ratio in the residual insoluble chromite. This specific action of chlorine on chromite can be described by the following equation:



Hematite (Fe_2O_3), being readily soluble in 10 hydrochloric acid can be removed by acid washing from the system, along with the acid soluble ferric chloride formed during the chlorination as shown by the following equation:



15 This relatively simple procedure, offers an interesting perspective to an easier access either to a chromite enriched in chromium.

The present invention therefore relates to a process for obtaining chromium enriched chromite from

chromite ores or chromite concentrates which comprises
the steps of:

- dry chlorinating the ores ore chromite
concentrates at a temperature between 400°C and 750°C to
5 produce chlorinated substrate containing acid soluble
ferric oxide, acid soluble ferric chloride and acid
insoluble chromium enriched chromite;
- digesting the obtained chlorinated
substrate with hydrochloric acid to dissolve the ferric
10 oxide and the ferric chloride; and
- filtering to recover said chromium enriched
chromite.

In another form of the invention, the dry
chlorinating step is conducted in the presence of sodium
15 chloride.

In one form of the invention, the chromite ores
are concentrated by gravimetric classification prior to
chlorination.

In another form of the invention, the digesting
20 step is carried out in the presence of heat.

Other objects and further scope of applicability of the present invention will become apparent from the detailed description given hereinafter. It should be understood, however, that this detailed 5 description, while indicating preferred embodiments of the invention, is given by way of illustration only, since various changes and modifications within the spirit and scope of the invention will become apparent to those skilled in the art.

10 IN THE DRAWINGS

Figure 1 is a block diagram illustrating the various steps of one embodiment of the process of the present invention.

DESCRIPTION OF PREFERRED EMBODIMENTS

15 One typical chromite ore used with the present invention is that from the Bushveld complex area in South Africa, containing approximatively 10% chromium of 45% chromite wherein the ratio of Cr to Fe is about 2 to 1.

20 Referring to the diagram, the ore is reduced to an appropriate size by grinding. It will be readily

understood that too coarse a material will prevent access to the material inside the particles and will slow down the reaction. On the other hand, very fine grinding involves significant cost. A value of particles of about 5 75 microns appears as a practical compromise between reactivity and cost of grinding.

Alternatively, the chromite ore may be upgraded prior to chlorination so as to give an enriched concentrate containing from 30% to 65% of chromium by 10 weight.

This ground material, either ore or concentrate, is then dried to less than 0.1% of free water and heated up to the appropriate temperature for a dry chlorine treatment, sodium chloride being preferably added at this stage. This temperature of dry chlorination has been found to be variable depending on the refractoriness of the ore under treatment. With certain ores, a temperature of 450°C has been sufficient. In other instances, higher temperatures (up to 700°C) 15 have been required to achieve similar recovery. The temperature of dry chlorination is an important factor in 20

the capacity of treatment of a given apparatus. This temperature must be high enough to ensure the desired reactions while too high a temperature may prove detrimental to the equipment and may induce undesirable reactions with chromite. It has been found that a temperature in the vicinity of 550°C is a preferred value. The ground ore can be heated to the selected temperature prior to contacting with chlorine or heated up in the chlorinator itself.

10 The hot ore is then introduced in the dry chlorinator, which is kept at the selected temperature, and a slow stream of chlorine or chlorine containing gas is circulated through the mass at constant temperature. It must be noted that the amount of chlorine required is
15 very small and amounts from 1.0 to 1.5 times the combined chlorine in the course of the dry chlorination. The amount of chlorine is relatively negligible, its consumption being related to the amount of reacting chromite and base metals, such as iron, nickel and copper
20 present in the starting ore. As an indicative estimate, it can be said that some of the base metal sulfides (Cu, Ni), up to 50 percent of the iron in the chromite and

less than one-tenth of one percent of the chromium in the chromite, will be converted into the corresponding soluble chlorides. In order to ensure an homogeneous distribution of the chlorine through the reacting mass,

5 the chlorine stream can be diluted by a carrier gas, such as nitrogen for example. The dry chlorination can be achieved on a continuous basis or batch-wise by simple percolation through the mass of the reacting gas or by the fluidization of the reacting bed or by renewal of the

10 surfaces in a rotating kiln. The contacting time required is relatively long (of the order of half an hour to two hours) depending on the nature of the ore, the degree of completion desired, the temperature used and, to some extent, on the granulometry of the ore. For sake

15 of simplicity of an apparatus which operates under rather aggressive conditions (chlorine at 600°C for example), a static bed of appropriate thickness has been found convenient. Since the material to be treated is to be loaded hot, the heating of the dry chlorination reactor

20 has to be just enough to compensate for heat losses of the system.

- 10 -

The volatiles leaving the dry chlorinator are directed to a condensing tower and quenched by a spray of hydrochloric acid at a concentration of 6M. The temperature in this tower is of the order of 50°C and the condensable are collected and carried down by the acid spray.

5 The solid left in the dry chlorinator after treatment is dumped, after cooling, in a digester containing the acid from the spray in the condensing tower, and is further digested, at 100°C, for one to several hours, the stirring of the mass being ensured by recirculation of the off gases of the condensation tower through the slurry. The off gases from the digester, mostly nitrogen, hydrochloric acid vapors, chlorine and 10 traces of sulfur compounds, are directed back to a gas treatment system after recycling condensed hydrochloric acid to the digester.

15 The temperature and duration of digestion in hydrochloric acid in the presence of chlorine must be adjusted in such a fashion as to ensure the complete dissolution of the soluble metal compounds. The heat 20

- increases the rate of such reactions, which could proceed nevertheless at room temperature but at a slower rate.
- For sake of completeness of dissolution as readily as possible of the metal, hot treatment is preferred over
- 5 cold treatment and a one to several hours of contacting is retained.
- Microscopic examination and diffraction analysis confirm the transformation of significant amounts of the ferrous oxide in chromite into hematite.
- 10 By acid leach in hydrochloric acid, the hematite can be removed while the chromium III oxide is left undissolved. This breakdown of the spinel structure has a weakening effect on the whole crystal which is rendered more friable. The material can be used as such, being an enriched chromium ore because of FeO removal, or it can
- 15 be further upgraded by taking advantage of the relatively high density of Cr₂O₃ as compared to the residual silicates initially present in the chromite ore. By application of gravimetric separation, a richer
- 20 concentrate in Cr₂O₃, can be obtained.

In summary, selective oxydation of chromite can lead to the production of hematite (Fe_2O_3), ferric chloride (FeCl_3) and chromium III oxide (Cr_2O_3) by rupture of the spinel structure of the starting chromite. Acid 5 leaching by hydrochloric acid can remove selectively the ferric oxide and chloride fraction, giving a significant enrichment in Cr_2O_3 of the insoluble residual chromite which can be further improved by gravimetric classification or appropriate physical separation of the 10 gangue initially found around the chromite crystal.

The solubilization of the iron oxide associated with the spinel structure of the chromite ($\text{FeO} \cdot \text{Cr}_2\text{O}_3$) thus can be achieved to a variable extent, allowing the removal of from five to sixty five percent of the FeO in 15 the starting chromite, giving an enrichment in chromite from a ratio of 2/1 to more than 4/1.

The range of enrichment is a function of temperature, duration of treatment and structure of the starting ore.

The solution separated from the insoluble chromite ore by filtration is directed to a distillation line or concentration apparatus, such as a reverse osmosis system, in order to recycle the hydrochloric acid at a concentration of 6M which corresponds to the azeotropic composition of the HCl-H₂O system. The bottoms of this distillation contain the iron, the chromium and the base metals (Ni, Cu, etc...) that have been dissolved in the course of the digestion of the dry-chlorinated ore. This material is directed to the gas treatment system which also receives the vapors of the digester.

EXPERIMENTAL

EXAMPLE 1

15 Samples were obtained from the chromite rich UG-2 layer of the Bushveld complex in South Africa. After grinding to 75 microns, a 35 gram portion of the original sample containing 0.4 to 0.6% added NaCl was subjected to a dry chlorination treatment at 560°C for 90 minutes. Before and after the chlorination experiments, solids were investigated by x-rays diffraction, optical

microscopy and scanning electron microscopy (SEM) coupled to an energy dispersive system (EDX).

Before chlorination, the main minerals present were: chromite, 45% with a Cr/Fe of 2/1; plagioclase feldspar, 45%; pyroxene, 10%; sulfides, 0.02%. After the chlorination experiments, the rupture of the spinel structure of the chromite was noted together with partial transformation (about 50%) of the chromite to hematite and Cr_2O_3 . These mineralogical modifications were indicated by: 1) a + 0.26° diffraction shift in the x-ray spectrum of $\text{FeO} \cdot \text{Cr}_2\text{O}_3$, and appearance of a new peak at 33.57°, both peaks being typical of the x-ray spectrums of hematite and Cr_2O_3 ; 2) SEM observations and EDX analyses of the grains which showed major signs of alterations revealed by the appearance of hematite and Cr_2O_3 crystals; 3) optical microscopy examination of the altered grains where the presence of hematite grains around the rims of the altered chromite grains could be clearly seen.

The inventors also noted that the plagioclase feldspar grains were untouched by the chlorination while

the pyroxene grains showed minimal alteration, these slight alterations being related to the presence, in the starting materials, of phyllosilicates inclusions in the pyroxenes.

5

EXAMPLE 2

The chlorinated product obtained from Example 1 was washed with 6M hydrochloric acid. In this solution, a series of 35 elements were analysed by ICP-AES. Only iron showed significative removal from the ore 10 by the chlorination process.

15

From these analysis, it can be seen that after dry chlorination and leaching with hydrochloric acid, the Cr₂O₃ is essentially intact and not dissolved. As to the iron, about 50% of this element is extracted either as the ferric chloride formed during the dry chlorination or by dissolution of the hematite. The Cr/Fe ratio is then increased to about 4/1 in the end product.

EXAMPLE 3

The chromite ore as described in Example 1 was 20 classified in a spiral so as to give concentrates

containing from 30 to 65% Cr₂O₃ by weight. These concentrates, after grinding to 75 microns, were treated as in Example I with similar increases in the Cr/Fe ratio.

5 Although the invention has been described above with respect with one specific form, it will be evident to a person skilled in the art that it may be modified and refined in various ways. For example, the grinding step may be carried out after the pre-heating step
10 illustrated in the diagram. It is therefore wished to have it understood that the present invention should not be limited in scope, except by the terms of the following claims.

The embodiments of the invention in which an exclusive property or privilege is claimed are defined as follows:

5

1. A process for obtaining chromium enriched chromite from chromite ores comprising the steps of:

10

- dry chlorinating said ores at a temperature from 400°C to 750°C to produce a chlorinated substrate containing acid soluble ferric oxide, acid soluble ferric chloride and acid insoluble chromium enriched chromite;

- digesting said chlorinated substrate with hydrochloric acid to dissolve said ferric oxide and said ferric chloride; and

15

- filtering to recover said chromium enriched chromite.

20

2. A process as defined in claim 1, further comprising the step of gravimetrically classifying said ores prior to said dry chlorinating step to obtain a chromite concentrate.

3. A process as defined in claim 1 or 2,
wherein said digesting step is carried out in the
presence of heat.

5 4. A process as defined in claim 3, wherein
said digesting step is conducted in the presence of heat
in the order of 100°C.

10 5. A process as defined in claim 4, wherein
gases resulting from said digesting step are directed to
a gas treatment system after recycling condensed
hydrochloric acid to said digesting step.

15 6. A process as defined in claim 1 or 2,
wherein said dry chlorinating step is conducted in the
presence of sodium chloride.

20 7. A process as defined in claim 6, comprising
the step of heating said ores prior to said dry
chlorinating step.

8. A process as defined in claim 6 or 7,
further comprising the step of drying said ores prior to
said dry chlorinating step; said sodium chloride being
introduced at said drying step.

5

9. A process as defined in claim 8, further
comprising the step of grinding said chromite ores prior
to said drying step.

10

10. A process as defined in claim 2, further
comprising the step of grinding said chromite ores after
said classifying step.

15

11. A process as defined in claim 9 or 10,
wherein said chromite ores are ground to a size of about
75 microns.

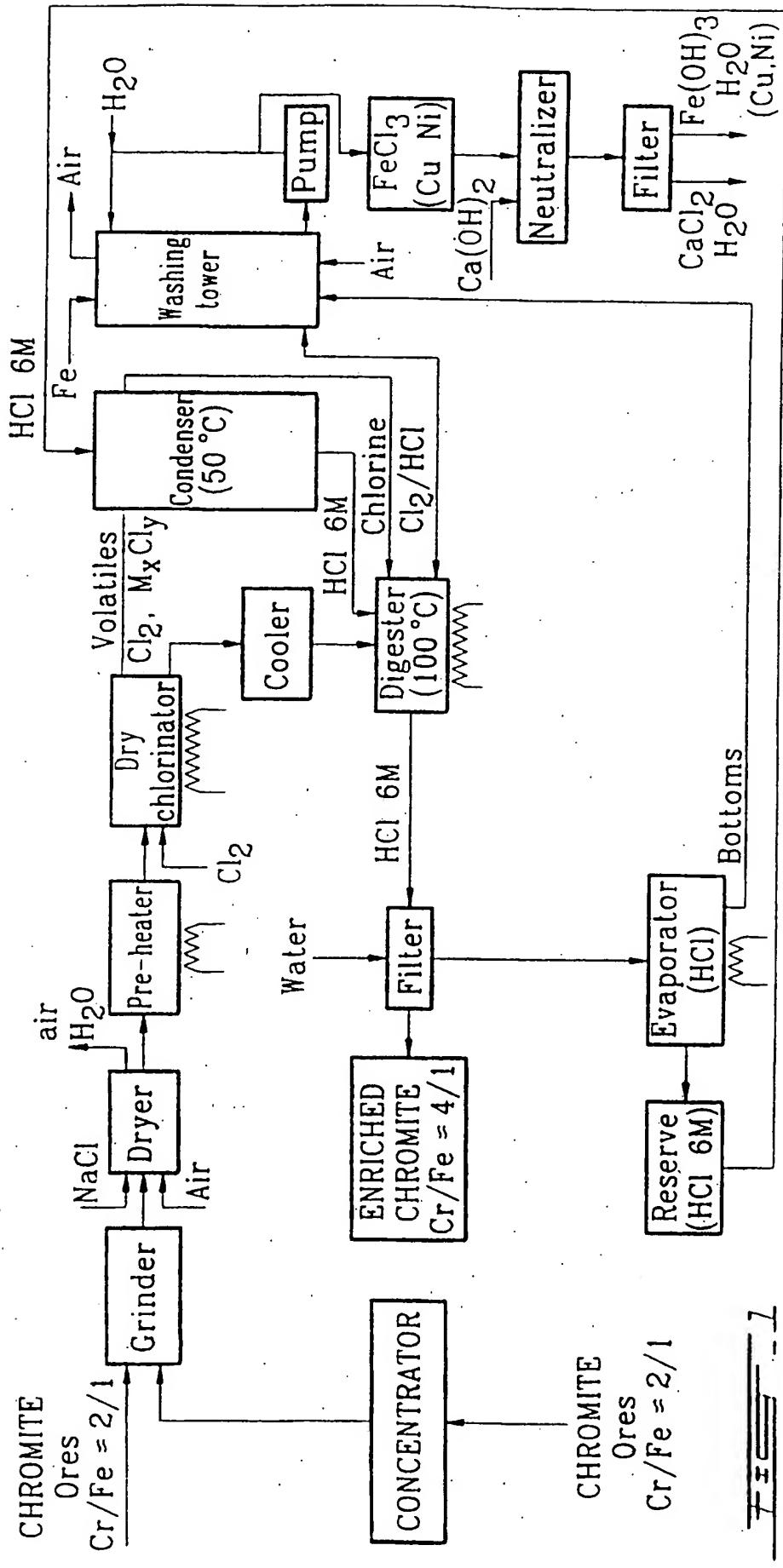
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12. A process as defined in claim 7,
comprising the step of cooling said chlorinated substrate
prior to said digesting step.

13. A process as defined in claim 1 or 2,
wherein said temperature is about 550°C.

14. A process as defined in claim 1 or 2,
further comprising the step of distillating a depleted
solution resulting from said filtering step to thereby
recycle the hydrochloric acid; bottoms of said
distillating step being directed to a system for treating
vapours from said digesting step.

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INTERNATIONAL SEARCH REPORT

Internal Application No

PCT/CA 96/00347

A. CLASSIFICATION OF SUBJECT MATTER
 IPC 6 C22B34/32 C22B1/08

According to International Patent Classification (IPC) or to both national classification and IPC

B. FIELDS SEARCHED

Minimum documentation searched (classification system followed by classification symbols)
 IPC 6 C22B

Documentation searched other than minimum documentation to the extent that such documents are included in the fields searched

Electronic data base consulted during the international search (name of data base and, where practical, search terms used)

C. DOCUMENTS CONSIDERED TO BE RELEVANT

Category	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
A	EP 0 016 516 A (LAPORTE INDUSTRIES LTD.) 1 October 1980 see page 2 - page 3; claims 1,8; example 1 ---	1,2,9-13
A	DE 11 35 668 B (WALTER M. WEIL) 30 August 1962 see claims 1-3 ---	1
A	DE 11 91 971 B (HAALMER CORPORATION) 29 April 1965 see claims 1-4 ---	1,3,4
A	GB 179 201 A (DYSON W.H. ET AL.) 28 July 1921 see claims 1-3; example 6 ---	1
A	BE 644 377 A (UNION CARBIDE CORPORATION) 15 June 1964 ---	1
	-/-	

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1 Date of the actual completion of the international search 30 January 1997	Date of mailing of the international search report 11.02.97
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INTERNATIONAL SEARCH REPORT

Internal	Application No
PCT/LA 96/00347	

C.(Continuation) DOCUMENTS CONSIDERED TO BE RELEVANT

Category	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
A	GB 2 001 042 A (TOYO SODA LTD.) 24 January 1979 -----	
A	US 3 892 639 A (LEAVENWORTH H.W. ET AL.) 1 July 1975 -----	

INTERNATIONAL SEARCH REPORT

In. based on patent family members

Internal Application No

PCT/LA 96/00347

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